

Original article

Nitrogen and phosphorus recovery from hemodialysis wastewater to use as an agricultural fertilizer

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ABSTRACT

Introduction: Hemodialysis wastewater contains high concentrations of ammonia nitrogen and phosphorus. Recovery of these nutrients as soil fertilizers represents an interesting opportunity to ensure a sustainable fertilizer supply.

Methods: In this paper, a simple method for recovering phosphorous and nitrogen as crystalline struvite [MgNH₄PO₄·6H₂O] is presented. An integrated cost model is also presented in order to create a positive business case.

Results: Recovery rates in form of struvite of 95% of PO₄³⁻-P and 23% of NH₄⁺-N were achieved with a profit.

Conclusion: To the best of our knowledge, this paper is the first to study the recovery of these naturally occurring minerals from hemodialysis wastewater. This offers great potential for the valorization of this type of wastewater.

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Recuperación de nitrógeno y fósforo del agua residual de la hemodiálisis para utilizar como fertilizante agrícola

RESUMEN

Introducción: El agua residual de la hemodiálisis contiene altas concentraciones de nitrógeno amoniacal y fósforo. La recuperación de dichos nutrientes como fertilizantes del suelo representa una oportunidad interesante para garantizar un suministro de fertilizantes sostenible.

Métodos: En este documento se presenta un método simple de recuperar fósforo y nitrógeno en forma de cristales de estruvita [MgNH₄PO₄·6H₂O]. También se presenta un modelo de costes integrado para crear un caso de negocio positivo.

Resultados: Se lograron unas tasas de recuperación en forma de estruvita del 95% de PO₄³⁻-P y el 23% de NH₄⁺-N, con beneficio.

Palabras clave:

Agua residual de la hemodiálisis

Valorización del agua residual

Fósforo

Nitrógeno

Eco-reciclado

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Conclusión: Según nuestros conocimientos, este documento es el primero que estudia la recuperación de estos minerales de origen natural del agua residual de la hemodiálisis, lo cual ofrece un gran potencial para la valorización de este tipo de aguas residuales.

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Introduction

Hemodialysis consumes huge volumes of water and produce large quantities of wastewater containing many potential resources like organic matter, nitrogen, and phosphorus.¹ Therefore, recovery and reuse of these nutrients as agricultural fertilizers is highly desirable.^{1,2} We have previously demonstrated that hemodialysis wastewater is a valuable resource that can provide fit-for-purpose water,³ energy,⁴ nutrients,^{1,2} and carbon emission savings.⁵

The discharge of wastewater in hemodialysis is high and could be estimated annually at approximately 98 million cubic meters over the world and 18 million cubic meters in United States.^{6,7} In our country, Morocco the discharge is estimated at 1 million cubic meters each year.^{6,7} In a world where demands for freshwater are ever growing, and where limited water resources are increasingly stressed by over-abstraction, pollution and climate change, neglecting the opportunities arising from improved wastewater management is nothing less than unthinkable.^{5,8,9}

Hemodialysis wastewater which contains a high amount of phosphorus and nitrogen would be a good source of struvite ($\text{MgNH}_4\text{PO}_4 \cdot 6\text{H}_2\text{O}$ – magnesium ammonium phosphate hexahydrate).¹⁰ This precipitate, due to its chemical characteristics, represents an effective alternative source of rock phosphate fertilizer for vegetables and plants growth.¹¹ Nitrogen and phosphorus in wastewaters are also a burning environmental issue. Recovering these elements from wastewater can also help reducing the amount of phosphorus entering the environment and thus lowering the environmental impact.¹¹

To the best of our knowledge, this paper is the first to study the recovery of this naturally occurring mineral from hemodialysis wastewater. This offers great potential for the valorization of this type of wastewater.

Materials and methods

Sampling and analyses

Water samples were obtained from a single dialysis facility. Wastewater was collected from the outflow pipe that drains hemodialysis effluent (spent dialysate) directly into the municipal sewage line. Samples were stored at 4 °C soon after sampling until used in struvite precipitation tests.

Samples were analyzed for the concentration of cations, anions, chemical oxygen demand (COD), ortho-phosphate (PO_4^{3-} -P) and total ammonium nitrogen (NH_4^+ -N). The cation concentrations were determined using an ICP-OES, type

Perkin Elmer Optima 3000 DV (Waltham, Massachusetts, USA). The anion concentrations were determined using an ion chromatography system, type Metrohm IC Compact 761 (Schiedam, The Netherlands). NH_4^+ -N was analyzed using test kit LCK 303. PO_4^{3-} -P was analyzed using test kit LCK 348 and COD was analyzed using test kit LCK 314 (all Dr. Lange, HACH, Loveland, Colorado, USA) in a spectrophotometer HACH XION 500 (HACH, Loveland, Colorado, USA). The biological oxygen demand (BOD) was determined using the OxiTop® system (WTW, Germany) over a period of 5 days at 20 °C.

Crystallizations experiments

A 5 l laboratory-scale, single-cell electrochemical batch reactor was used for struvite production (Fig. 1). The pH and temperature values were monitored through online probes. In all experiments, magnesium chloride hexahydrate ($\text{MgCl}_2 \cdot 6\text{H}_2\text{O}$) was added to meet a molar ratio $[\text{Mg}^{2+} : \text{Ca}^{2+} > 2]$ and $[\text{Mg}^{2+} : \text{PO}_4^{3-} > 1]$, which were selected based on data reported by Li et al.¹² and Liu et al.¹³ who found struvite crystals with high purity and high phosphorus recovery when using these molar ratios. Crystallization was attained at electric current density of 55 A m^{-2} . The obtained struvite cake from the process was dried at room temperature to form a powder.

Struvite precipitate characterization

The crystalline nature and the semi quantitative composition were determined by X-ray diffraction (XRD; Bruker D2 Phaser), using struvite standard X-ray diffraction patterns. Phosphorus precipitation in the crystallizer was assessed using “The percentage of precipitated phosphorus as struvite” (P_{MAP} , %).

P_{MAP} was calculated as the ratio of the number of precipitated mmoles of struvite ($n(\text{MAP})$) (mmol), which was assumed to be the lowest value between the precipitated mmoles of Mg^{2+} , PO_4^{3-} -P and NH_4^+ -N and the precipitated mmoles of PO_4^{3-} -P in the solution, as shown in the equation below:¹⁴ $P_{\text{MAP}} (\%) = \frac{n(\text{MAP})_{\text{precipitated}}}{(\text{PO}_4^{3-}\text{-P})_{\text{precipitated}}} \times 100$

Results

Characterization of hemodialysis wastewater

The characteristics of the wastewater are shown in Table 1; the average concentration of PO_4^{3-} -P and NH_4^+ -N was 13.2 mg L^{-1} and 4.2 mg L^{-1} respectively. The samples had an average pH of 7.53. The BOD was found to be approximately 8.13 mg L^{-1} , and the COD was 1053 mg L^{-1} .



Fig. 1 – Experimental equipment for struvite crystallization.

Evaluation of phosphorus and nitrogen recovery

Under optimal conditions, the removal efficiencies of PO_4^{3-} -P and NH_4^+ -N in struvite precipitation were analyzed as approximately 95% and 23%, respectively (Table 2). The phosphorus removal as struvite was similar at the three pH conditions evaluated (i.e., pH 8, 9 and 10). Although, the removal of NH_4^+ -N increased as the pH value increased (Fig. 2). The nitrogen removal can be explained as a combination of the precipitation and volatilization processes, the latter favored under well-mixing conditions at higher pH levels.¹⁵ Temperature has a relatively less significant effect on struvite precipitation than the pH level. However, the temperature strongly influences the efficiency of phosphate removal.

Precipitates formed in the crystallization process

The X-ray diffractogram obtained in the analysis of the solids precipitated shows a good correlation between the peaks of

the diffractogram obtained for the solid collected in the reactor and the peak of the struvite pattern which confirms that the solid formed was mainly struvite. Phosphorus precipitation in the crystallizer was higher at a pH of 9 and 10 than at a pH of 8, and the mean PMAP was 82.8%.

Economic efficiency of struvite production

We did an estimate of the financial efficiency of struvite production based on a tailor-designed system for a medium sized dialysis facility working with 20 machines filled to capacity and 2 shifts/day and generating approximately 3000 l of wastewater (150 l of waste dialysate is being generated during each dialysis session: assuming a DFR of 500 ml/min, 120 L of dialysate is produced during a typical 4H hemodialysis session + 30 L of water needed for chemical disinfection of the hemodialysis monitor⁵). The system was designed to produce struvite on a regular basis (2.4 kg of struvite can be produced daily). The system consists of wastewater collection tank; a

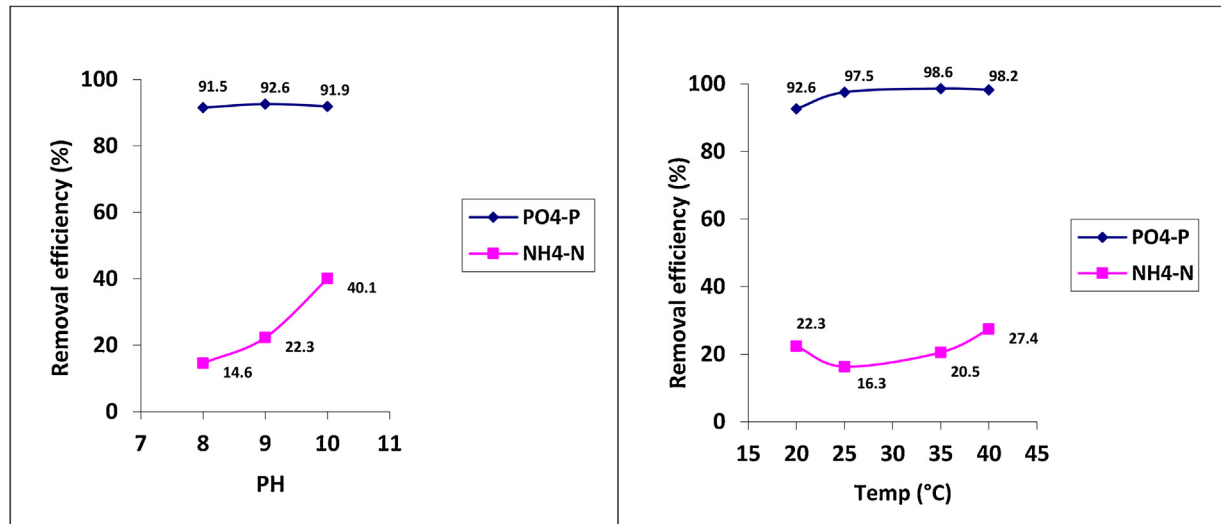


Fig. 2 – Effect of pH and temperature on phosphorus and nitrogen removal.

Table 1 – Results of physico-chemical characterization of effluents from hemodialysis. The average was obtained from four different samples obtained on different days.

Composition	Average	Range
Temperature (°C)	23.5	22–25
pH	7.53	6.91–8.15
COD (mgL ⁻¹)	1053	986–1120
BOD (mgL ⁻¹)	8.13	7.98–8.28
NH ₄ ⁺ -N (mgL ⁻¹)	4.2	3.05–5.35
PO ₄ ³⁻ -P (mgL ⁻¹)	13.2	12.32–14.08
Sodium (mgL ⁻¹)	3289	3243.4–3334.6
Potassium (mgL ⁻¹)	93.7	88–99.4
Magnesium (mgL ⁻¹)	52.1	49.8–54.4
Calcium (mgL ⁻¹)	86.2	81.9–90.5
Alkalinity (mgL ⁻¹ as CaCO ₃)	1715	1667–1763

COD (chemical oxygen demand) is the amount of dissolved oxygen that must be present in water to oxidize chemical organic materials.

BOD (biochemical oxygen demand) is the amount of dissolved oxygen used by microorganisms in the biological process of metabolizing organic matter in water.

struvite reactor for struvite precipitation and a pilot scale rotating biological contactor (RBC) to treat a small fraction of the effluent from struvite production before disposing it to the

Table 3 – Operating parameters for economic evaluation of struvite production from hemodialysis wastewater.

Parameters	Results
Reactor size (l)	500
Cycles per day	6
Struvite recovery efficiency (%) (PO ₄ ³⁻ -P/NH ₄ ⁺ -N)	90/20
Daily struvite production (kg)	2.44
Yearly struvite production (kg)	760
Molar Mg:P ratio	1.1
Yearly required MgSO ₄ (kg) ¹⁶	45
Yearly required MgSO ₄ evaluation was performed according to the method by Agudosi et al. ¹⁶	

environment (Table 3). Data on costs and benefits are shown in Table 4.

Discussion

Recognition that hemodialysis wastewater is an economic resource capable of supplying water,³ nutrients,^{1,2} energy⁴ and other valuable materials and services^{4,5} has become a major driving force to improve effective wastewater management.⁵ Each year, for instance, approximately 98 million cubic meters of hemodialysis wastewater are generated globally.^{6,7} Theo-

Table 2 – Removal efficiency of phosphorus and nitrogen.

T (°C)	20	20	20	25	35	40
pH	8	9	10	9	9	9
Removal efficiency (%)						
PO ₄ ³⁻ -P	91.5 ± 0.2	92.6 ± 0.1	91.9 ± 0.3	97.5 ± 0.2	98.6 ± 0.0	98.2 ± 0.1
NH ₄ ⁺ -N	14.6 ± 1.4	22.3 ± 0.7	40.1 ± 0.4	16.3 ± 1.1	20.5 ± 0.4	27.4 ± 1.2
MAP precipitates						
PMAP (%)	70.4 ± 0.3	83.4 ± 1.6	82.8 ± 0.9	92.5 ± 0.4	77.3 ± 1.8	90.1 ± 1.0
Mass (g)	3.9 ± 0.0	3.7 ± 0.1	4.2 ± 0.1	4.4 ± 0.0	4.1 ± 0.2	4.1 ± 0.1

PMAP: the percentage of phosphate as struvite.

Table 4 – Estimating cost of nutrients recovery as struvite.

Operations parameters	Results
Equipment cost (USD)	1350
Wastewater storage tank: 3 m ³ (USD)	180
Additional costs (fittings, pipes, etc.) (USD)	80
Estimated total investment (USD)	1610
Required MgSO ₄ price (USD/kg) ¹⁷	0.33
Operations costs (USD/year)	100.3
Maintenance costs (USD/year)	48
Operating duration (year)	10
Struvite market price (USD/kg) ¹⁸	0.8
Annual cash inflow (USD)	608
Payback period (month)	42

Prices were calculated according to Refs. 16 and 17.

retically, the resources embedded in this wastewater would be enough to irrigate and fertilize hundreds of thousands of hectares of crops.

This effluent can also maintain considerable thermal energy quantities, which is discharged to the sewer system with temperature ranging from 20 to 25 °C. It is estimated that 1698 GWh per year of thermal energy is lost in sewers in dialysis units all over the world and 314 GWh in the US (the specific thermal capacity of wastewater is: 1.16 kWh/m³ × K; the wastewater in the effluent will be cooled down to 5 °C, so that 15 K can be extracted).¹⁹

Globally, hemodialysis wastewater is estimated to contain enough energy to heat 141,500 homes (the average home requires around 12,000 kWh of heat/year),²⁰ with an annual fuel cost savings of 118 million Euros if recovered by using technologies like heat exchangers and reused to satisfy heating demands (12,000 kWh heat demand/3 kW heat production per unit of electricity = 4000 kWh of electricity). Average residential electricity price in Europe is 0.21 euros).²¹

Hemodialysis wastewater maintains good amount of carbon, nitrogen and phosphorus, of which have large impacts on the environment. Wastewater from hemodialysis can disrupt aquatic ecosystems with deleterious impacts on aquatic biodiversity, landscapes and recreational opportunities.²² Recovery of nutrients from wastewater can alleviate major environmental problems related to nutrient pollution in ground and surface water sources.²¹ In this pilot study, recovery rates of 95% of PO₄³⁻-P and 23% of NH₄⁺-N were achieved.

Application of struvite in the agricultural sector promises to be a profitable investment. It has been demonstrated that generating 1 kg of struvite per day is enough to fertilize 2.6 ha of arable land by applying phosphorus (as P₂O₅) at a rate of 40 kg/ha year.²⁰ In this study we were able to demonstrate that an hemodialysis facility with 20 chairs and 2 shifts/day could generate approximately 2.4 kg of struvite per working day with a profit, and a possibility to fertilize 5.2 ha of arable land (estimation based on 6 working days/week). Regarding the environmental cost, the use of wastewater in lieu of synthetic fertilizers can results in an important carbon emissions saving. De Vries et al., have estimated that the use of struvite as fertilizer can results in saving of -0.35 kg CO₂ eq. kg⁻¹ of struvite.²³

Conclusion

The recovery of phosphorus and nitrogen from wastewater is a model for sustainable innovation in hemodialysis. Removing nutrients from where they should not be and using them to create a new generation of enhanced-efficiency fertilizer is the smart thing to do economically and the right thing to do environmentally.

Conflict of interests

The authors declare they have no conflict of interest.

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